



Lecture (7-8) PID Controller

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- Control Systems Course, professor Aniket Khandekar, Zeal college of engineering and Research, Pune.
- Gopal, M. Control Systems_ Principles and Design 3rd edition-Tata McGraw Hill Publishing Co. Ltd. (2008)
- Modern Control Systems, Richard C. Dorf and Robert H. Bishop, Prentice Hall, 12th edition, 2010, ISBN-10: 0-13-602458-0
- Modelling, Dynamics and Control, University of Sheffield, John Anthony Rossiter.
- https://www.wevolver.com/article/mastering-pid-tuning-thecomprehensive-guide

Introduction This introduction will show you the <u>characteristics</u> of the <u>each</u> of <u>proportional</u> (P), the <u>integral</u> (I), and the <u>derivative</u> (D) <u>controls</u>, and how to use them to <u>obtain</u> a <u>desired response</u>.

□ In this lecture, we will consider the following unity feedback system:



- □ **<u>Plant</u>**: A system to be controlled
- Controller: Provides the excitation for the plant; Designed to control the overall system behavior

The PID controller

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□ The transfer function of the PID controller looks like the following:

$$G_c(s) = K_p + K_D s + \frac{K_I}{s}$$

- Kp = Proportional gain
- K_I = Integral gain
- Kd = Derivative gain



The PID controller



- □ First, let's take a look at how the PID controller works in a closed-loop system using the schematic shown above. The variable [E(s)] represents the <u>tracking error</u>, the <u>difference</u> <u>between</u> the <u>desired input</u> value [R(s)] and the <u>actual output</u> [C(s)].
- □ This <u>error</u> signal (e) will be <u>sent</u> to the <u>PID</u> controller, and the <u>controller</u> <u>computes</u> both the <u>derivative</u> and the <u>integral</u> of this <u>error</u> <u>signal</u>.
- □ The <u>signal [U(s)]</u> just past the controller is now equal to the proportional gain (Kp) times the magnitude of the error plus the integral gain (Ki) times the integral of the error plus the derivative gain (Kd) times the derivative of the error.

$$u(t) = K_p e(t) + K_I \int e(t) dt + K_D \frac{d e(t)}{dt}$$

- This signal (u) will be <u>sent</u> to the <u>plant</u>, and the <u>new output</u> will be <u>obtained</u>. This new output will be <u>sent</u> <u>back</u> to the sensor again to find the <u>new error signal</u> (e). The controller takes this new error signal and computes its derivative and its integral again.
- □ This process goes on and on.

The PID controller

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The characteristics of

- □ A proportional controller (Kp) will have the effect of <u>reducing</u> the <u>rise</u> time and will <u>reduce</u>, but <u>never</u> eliminate, the <u>steady-state</u> error.
- An <u>integral</u> control (Ki) will have the effect of <u>eliminating</u> the <u>steady-state</u> error, but it may make the <u>transient response</u> worse.
- □ A <u>derivative</u> control (Kd) will have the effect of <u>increasing</u> the <u>stability</u> of the system, <u>reducing</u> the <u>overshoot</u>, and <u>improving</u> the <u>transient</u> <u>response</u>.
- Effects of each of controllers Kp, Kd, and Ki on a closed-loop system are summarized in the table shown below.

Decrease
liminate
all Change

Proportional Controll



$$P = K_p \cdot E_p + P_o$$

where

P = controller output, including error P_o = controller output without error (%) E_P = error signal in proportional control action K_P = proportional controller gain or proportional constant between error and controller output.

Integral Controller









In the context of integral control, <u>windup</u> refers to a <u>situation</u> where the <u>integral term continues</u> to <u>accumulate</u> an <u>error</u> even <u>when</u> the <u>system</u> has <u>reached</u> a <u>saturation limit</u> (maximum or minimum output). <u>Windup</u> can <u>occur</u> when the <u>integral action</u> is <u>unable</u> to <u>correct</u> the <u>error</u> due to <u>constraints on the manipulated</u> <u>variable</u>. This situation can <u>lead</u> to overshooting and prolonged settling times.

How a PID controller work



. Example of what happens in a proportional-plus-Integral control system when the setpoint is changed suddenly.





K_d=T_d [min]

14

PID Circuit:





- XOP2 (Proportional): -(RP2/RP1)(Verr)
- XOP3 (Derivative): -(RD*CD)*(d(VERR)/dt)
- XOP4 (Integral): -(1/RI*CI)*(∫Verr dt)
- XOP5 (Summer): [(R7/R4)(XOP2) + (R7/R5)(XOP3) + (R7/R6)*(XOP4)]
- XOP6 (Inverter): -(R9/R8)*(XOP5)

Example Problem



□ Suppose we have a simple mass, spring, and damper problem.

The modeling equation of this system is

$$M\frac{d^2 x(t)}{dt^2} + f_v \frac{dx(t)}{dt} + Kx(t) = f(t)$$

$$\frac{X(s)}{F(s)} = \frac{1}{M s^2 + f_v s + K}$$

- □ Let
 - M = 1kg
 - *f*_v = 10 N.s/m
 - k = 20 N/m
 - F(s) = 1 = unit step





Open-loop step response

□ Let's first view the open-loop step response.



- □ Create a new m-file and add in the following code:
 - >> num=1;
 - >> den=[1 10 20];
 - >> step (num,den)
- Running this m-file in the Matlab command window should give you the plot shown below.

Open-loop step response

- The <u>DC gain</u> of the plant transfer function is 1/20, so <u>0.05</u> is the <u>final value</u> of the output to an unit step input. This corresponds to the <u>steady-state error</u> of <u>0.95</u>, quite <u>large</u> indeed.
- □ Furthermore, the <u>rise time</u> is about <u>one second</u>, and the <u>settling time</u> is about <u>1.5</u> seconds.
- Let's design a <u>controller</u> that will <u>reduce</u> the <u>rise</u> <u>time</u>, reduce the <u>settling</u> <u>time</u>, and <u>eliminates</u> the <u>steady-state</u> <u>error</u>.







□ The closed-loop T.F is

$$\frac{C(s)}{R(s)} = \frac{K_p}{s^2 + 10 s + (20 + K_p)}$$

Let the proportional gain (Kp) equals 300 and change the m-file to the following:
No Kp = 300:

- >> Kp =300;
- >> num = [Kp];
- >> den = [1 10 20+Kp];
- >> t = 0:0.01:2;
- >> step (num,den,t)

Closed Loop with P-Controller

Running this m-file in the Matlab command window should give you the following plot.

The plot shows that the proportional controller reduced both the rise time and the steady-state error, increased the overshoot, and decreased the settling time by small amount.



Closed Loop with PD-Controller



□ The closed-loop T.F is

$$\frac{C(s)}{R(s)} = \frac{K_p + K_D S}{s^2 + (10 + K_D) s + (20 + K_p)}$$

Let Kp equals 300 and Kd equals 10, then change the m-file to the following: >> Kp =300; KD=10; >> num = [KD Kp]; >> den = [1 10+KD 20+Kp];

- >> t = 0:0.01:2;
- >> step (num,den,t)

Closed Loop with PD-Controller

Running this m-file in the Matlab command window should gives you the following plot.

The plot shows that the derivative controller reduced both the overshoot and the settling time, and had small effect on the rise time and the steady-state error.



Closed Loop with PI-Controller



Let Kp equals 300 and Ki equals 70, then change the m-file to the following: >> Kp = 300; KI = 70;

- >> num = [Kp KI];
- >> den = [1 10 20+Kp KI]
- >> t = 0:0.01:2;
- >> step (num,den,t)

Closed Loop with PI-Controller

Running this m-file in the Matlab command window should gives you the following plot.
Closed-Loop Step: Kn=30 Ki=70

We have reduced the proportional gain (Kp) because the integral controller also reduces the rise time and increases the overshoot as the proportional controller does (double effect). The above response shows that the integral controller eliminated the steady-state error.





>> num =
$$[K_D K_p K_l];$$

>> den = $[1 \ 10 + K_D \ 20 + K_p K_l];$

>>
$$t = 0.0 01.2$$

>> step (num,den,t)

Closed Loop with PID-Controller

Running this m-file in the Matlab command window should gives you the following plot.

Now, we have obtained the system with no overshoot, fast rise time, and no steady- state error.





PID Tuning:

□ What is the process of PID tuning?

- Choosing the proper values for P, I, and D is called "PID Tuning".
- Used to get a desired and stable response of the controlled variable.
- PID Tuning Methods:
 - 1) There are lots of methods.
 - 2) We will use three basic and common methods:

1) Manual method.

2) Ziegler-Nichols method.

1) Open-Loop method.

2) Closed-Loop method.

3) Using MATLAB.

PID Tuning (Manual method):

□ Step-by-step guide to manual PID tuning:

- 1. Set all gains to zero (Kp = 0, Ki = 0, Kd = 0).
- 2. Increase Kp until the system responds to setpoint changes with acceptable speed, but without excessive overshoot.
- 3. Increase Ki gradually to eliminate steady-state error. Watch for oscillations or instability.
- 4. If needed, introduce Kd to reduce overshoot and dampen oscillations. Be cautious, as too much derivative action can introduce noise sensitivity.
- 5. Fine-tune all parameters iteratively, making small adjustments and observing the system response.
- 6. Test the system with various setpoints and disturbances to ensure robust performance.

	RISE TIME	OVERSHOOT	SETTLING TIME	Steady-State Response
Кр	Decrease	Increase	Small Change	Decrease
Ki	Decrease	Increase	Increase	Eliminate
Kd	Small Change	Decrease	Decrease	Small Change

PID Tuning (Manual method):



	RISE TIME	OVERSHOOT	SETTLING TIME	Steady-State Response
Кр	Decrease	Increase	Small Change	Decrease
Ki	Decrease	Increase	Increase	Eliminate
Kd	Small Change	Decrease	Decrease	Small Change



Ziegler-Nichols Tuning Rule Based on Step Response of Plant (First Method)

Type of Controller	K_p	$T_i = 1/K_i$	$T_d = \mathbf{K}d$
Р	$\frac{T}{L}$	∞	0
ы	$0.9 \frac{T}{L}$	$\frac{L}{0.3}$	0
PID	$1.2 \frac{T}{L}$	2 <i>L</i>	0.5L

32



PID Tuning -Ziegler-Nich

□ A practical walkthrough of the Ziegler-Nichols method:

- 1. Disable integral and derivative actions (set $Ti = \infty$ and Td = 0).
- 2. Increase Kp=Kc until the system exhibits sustained oscillations. This gain is the ultimate gain (Ku)>>Calculate Ku manually or using Routh method.
- 3. Measure the period of oscillations (Tu).
- 4. Calculate PID parameters based on Ziegler-Nichols method:

Control type	Кр	Ki	Kd
Р	0.50Ku	—	—
PI	0.45Ku	0.54Ku/Tu	—
PID	0.60Ku	1.2Ku/Tu	3KuTu/40

PID Tuning (Ziegler-Nichols method) Example1:





PID Tuning (Ziegler-Nichols method) Example1:

Manual Method:

Kp = 0.60 x Kc→Kp = 0.6 x 7.5→Kp = 4.5 Ki=1.2xKc/Tu=1.2x7.5/1.985→Ki=4.53 Kd=3x Kc x Tu/40=3x7.5x1.985/40→Kd=1.117

Control type	Кр	Ki	Kd
Р	0.50Ku	—	
PI	0.45Ku	0.54Ku/Tu	—
PID	0.60Ku	1.2Ku/Tu	3KuTu/40



PID Tuning (Ziegler-Nicholsmethod) Example1:

🚹 Block Parameters: PID	O Controller1	\times
PID Controller		^
This block implements or reset, and signal tracking	continuous- and discrete-time PID control algorithms and includes advanced features such as anti-windup, exter ng. You can tune the PID gains automatically using the 'Tune' button (requires Simulink Control Design).	mal
Controller: PID	✓ Form: Parallel	-
Time domain:		
Continuous-time		
○ Discrete-time		
Main PID Advanced	d Data Types State Attributes	
Controller parameters		
Source:	internal Compensator formula	ula
Proportional (P):	4.5	
Integral (I):	4.53	
Derivative (D):	1.117 $\vdots \qquad P+I\frac{1}{s}+D\frac{1}{1+N\frac{1}{s}}$	-
Filter coefficient (N):	100	;
Select Tuning Method:	Transfer Function Based (PID Tuner App)	~
0	OK Cancel Help A	Apply

37

PID Tuning (Ziegler-Nichols method) Example1:





PID Tuning (Ziegler-Nicholsmethod) Example1:

🚹 Block Parameters: PID (Controller1						×
PID Controller							^
This block implements co reset, and signal tracking	ontinuous- and di g. You can tune ti	screte-time PID cor ne PID gains autom	ntrol algorithms an atically using the	d includes advan Tune' button (i	ced features suc requires Simulin	ch as anti-windup, exte k Control Design).	rnal
Controller: PID			▼ Form:	Parallel			-
Time domain:							
Ontinuous-time							
○ Discrete-time							
Main PID Advanced	Data Types	State Attributes					
Controller parameters							
Source:	internal				•	Compensator form	iula
Proportional (P):	4.5				:		
Integral (I):	4.53				:	1 N	
Derivative (D):	1.117				:	$P+I\frac{1}{s}+D\frac{I}{1+N}$	ī
Filter coefficient (N):	100				:	1111	s
Select Tuning Method:	Transfer Functio	n Based (PID Tune	r App)	-	Tune		~
				OK	Cancel	Help	Apply

39

PID Tuning using MATLAB PDTuner (Example1):



Controller Parameters: P = 0.7284, I = 0.1163, D = 0.8243, N = 6.809

PID Tuning using MATLA PID Tuner(Example1):

	•			
Top/Bottom Shrink Tabs to F	Fit			
Custom				
TILES DOCUMENT TABS				
Step Plot: Reference tracking 🛛 🗶				
Sten Blat: Ba	forence tre ching			
1.8		Controller Parameters		
1.0	Tuned response		Tuned	Block
1.6	Block response	Р	0.72843	4.5
1.1		1	0.11633	4.53
1.4		D	0.82433	1.117
		N	6.8095	100
12				
8 1				
를 지난 동안 것 같아.		Performance and Rob	ustness	
Q 0.8			Tuned	Block
		Rise time	1.02 seconds	0.382 seconds
0.6		Settling time	11.7 seconds	10.7 seconds
		Overshoot	10.2 %	66.2 %
1		Peak	1.1	1.66
0.4			24 10 @ 0.76 17	-10.2 dB @ 1.36 rad/
0.4		Gain margin	24 dB @ 9.76 rad/s	10/2 00 @ 1.50100/.
0.4		Gain margin Phase margin	24 dB @ 9.76 rad/s 69 deg @ 1.25 rad/s	17.7 deg @ 2.49 rad/

41



PID Tuning (Ziegler-Nicholsmethod) Example2:





42

PID Tuning (Ziegler-Nichols method) Example2:





PID Tuning (Ziegler-Nicholsmethod) Example2:

Manual Method:

Kp = 0.60 x Kc \rightarrow Kp = 0.6 x 30 \rightarrow Kp = 18 Ki=1.2xKc/Tu=1.2x30/2.816 \rightarrow Ki=12.78 Kd=3x Kc x Tu/40=3x30x2.816/40 \rightarrow Kd=6.336

Control type	Кр	Ki	Kd
Р	0.50Ku	—	
PI	0.45Ku	0.54Ku/Tu	—
PID	0.60Ku	1.2Ku/Tu	3KuTu/40

PID Tuning (Ziegler-Nicholsmethod) Example2:



Hardware Demo of a Digita PID Controller:

This is a physical demonstration of a PID controller controlling the angular position of the shaft of a DC motor. It was designed as a teaching tool to show the effects of proportional, integral, and derivative control schemes as well as the effect of saturation, anti-windup, and controller update rate on stability, overshoot, and steady state error. Enjoy!

> Gregory Holst December 2015 http://gregoryholst.com

https://www.youtube.com/watch?v=fusr9eTceEo/manara.edu.sy/